

COMPRESSED AIR IN WASTEWATER TREATMENT

BY SCOTT VAN ORMER AND HANK VAN ORMER
FOR THE COMPRESSED AIR CHALLENGE®



When you hear “water treatment” what is the first thing that comes to mind? Sewer water treatment? Certainly this is often the case. Municipal water treatment is classic water treatment requiring aeration, agitation and continuous fluid movement.

Wastewater Municipal Water & Sewage Treatment:

- Compressed air used for agitation to keep solids in suspension
- Compressed air is often needed to supply oxygen support to the processing bacteria

Air pressure required depends on:

- Liquid/slurry depth
- Actual water head pressure 2.31 feet equals 1 psig
- For estimating we use .5 psig per foot of head of H₂O — specific gravity of water is 1.0. Mixtures and slurries with higher specific gravity will have greater head pressure

COMPRESSORS OFTEN USED FOR WATER TREATMENT AERATION AND AGITATION

AIR COMPRESSORS	ACFM (APPROX.)	HORSEPOWER (APPROX.)	COOLING TYPE	PSIG (APPROX.) * POSSIBLE HIGHER PRESSURE	LUBRICATED OR NON-LUBRICATED
Reciprocating Single or 2-Stage	<1 to 5,000 acfm	<1 hp to 1,000 hp	Air <60 hp or Water >60 hp	30-75 psig 90-150* psig	Lubricated or Non-lubricated
Single-Stage Lubricated Rotary Screw	15 to 3,000 acfm	5 hp to 700 hp	Air or Water	90-150*	Lubricated
2-Stage Lubricated Rotary Screw	500 to 3,100 acfm	100 hp to 600 hp	Air or Water	90-200*	Lubricated
Oil-Free Rotary Screw Single or 2-Stage	75 to 4,200 acfm	40 hp to 900 hp	Air or Water	28-50 90-125*	Non-lubricated
Centrifugal Single to 3-Stage	375 to 5,000 acfm	75 hp to 1,000 hp	Air or Water	28-60 90-150*	Non-lubricated

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The object of this article is to look at some very typical industrial water treatment processes and various compressed air and energy savings projects that have worked well for our clients over the years. The basic fundamentals with regard to compressed air usage are similar to municipal water treatment — a good starting point.

Disclaimer: This data is not intended to be complete enough to select wastewater air. It is designed to give the reader an overall view of the basic operating parameters of each type.

There are many types of blowers (rotary vane, liquid ring, etc.) used in industry, particularly in the smaller sizes. As in most air and gas compression equipment, larger, well applied central units may well prove to be the most energy efficient solution when conditions dictate. Each opportunity needs a specific evaluation.

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LOW PRESSURE AIR (LESS THAN 30 PSIG) BLOWERS

BLOWERS	ACFM (APPROX.)	HORSEPOWER (APPROX.)	COOLING TYPE	PSIG (APPROX.) * POSSIBLE HIGHER PRESSURE	LUBRICATED OR NON-LUBRICATED
Regenerative Dynamic Compression Blower (Figure 1)	250 to 1,350 acfm **	5 hp to 30 hp	Air	2-4.5	Non-lubricated
Centrifugal Dynamic Compression Blower Single-Stage (Figure 2)	20 to 45,000 acfm	10 hp to 1,000 hp ***	Air or Water	.3-28	Non-lubricated
Positive Displacement Straight Lobe Single and 2-Stage (Figure 3)	75 to 2,500 acfm	4 hp to 250 hp	Air	4-12*	Non-lubricated
Positive Displacement Helical Lobe Single and 2-Stage (Figure 4)	400 to 6,500 acfm	20 hp to 650 hp	Air	10-18*	Non-lubricated
Positive Displacement "Claw" Type Lobe Single-stage (Figure 5)	40 to 350 acfm	5 hp to 40 hp	Air	18-30	Non-lubricated

** Larger units are available

*** Note: With single-stage centrifugal blowers the ability to deliver higher pressures increases with the flow volume. The required horsepower to produce the flow varies with flow and pressure selection. The air "mass flow" units and the driving power is a direct function of the mass flow or weight of the air.

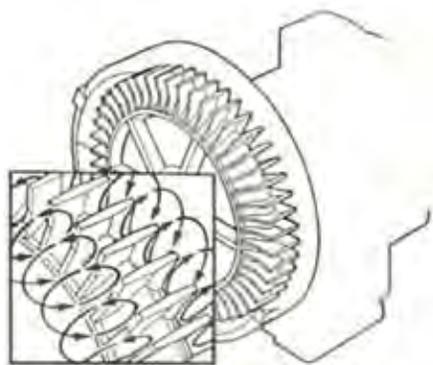


Figure 1. Regenerative Dynamic Compression Blower



Figure 2. Centrifugal Dynamic Compression Blower Single-stage



Figure 3. Positive Displacement Straight Lobe Single and 2-Stage



Figure 4. Positive Displacement Helical Lobe Single-stage

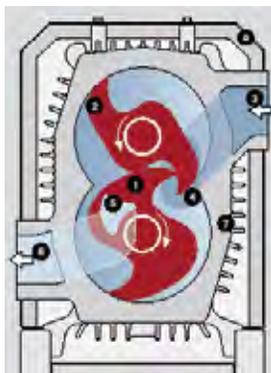


Figure 5. Positive Displacement "Claw" type Lobe Single-stage

The lower the pressure, the lower the energy cost per scfm of delivered volume of compressed air with the same type and class of compressed air operating equipment. This is generally true regardless of the type of compressed air generating unit as long as the pressure flow is within a given units operating parameters.

This looks somewhat simple — just identify the minimum acceptable pressure that works and the required or current actual compressed air flow being used. Then, select the appropriate blower or air compressor. In an existing plant or operation this can often be challenging since many operators do not have nor know this information.

TYPICAL OPERATING COST FOR 500 CFM AT VARIOUS PRESSURES (BASED ON \$.06/KWH AND 8,000 HRS/YEAR)		
ELECTRICAL ENERGY COST TO PRODUCE:	500 cfm at 100 psig	\$43,000
	500 cfm at 50 psig	\$26,000
	500 cfm at 15 psig	\$18,000
	500 cfm at 7 psig	\$8,000

In the field you can measure the flow and inlet pressure, but to accurately estimate the probable lowest usable discharge pressure you will need to know the specific gravity of the solution and the overall height of the liquid or slurry material (depth) to establish the “head pressure” to be overcome.

Unlike a municipal sanitary sewer wastewater treatment facility this data is often not only not readily available but also may well vary over time and application in the industrial wastewater environment.

Generally compressed air is combined with some type of liquid or slurry pump appropriate to handle the material. Often this is an air operated double diaphragm pump due to its simple design and versatile application parameters. They are also relatively quick to repair and/or change. Electric driven pumps are often not even considered.



There are three primary uses of compressed air in all wastewater treatment applications:

- Aeration to supply the processing bacteria with oxygen support
- Agitation to keep the solids in suspension and,
- A continuous, driving pump to move the material.



The lower the pressure, the lower the energy cost per scfm of delivered volume of compressed air with the same type and class of compressed air operating equipment.

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Basic Methods of Aeration / Agitation

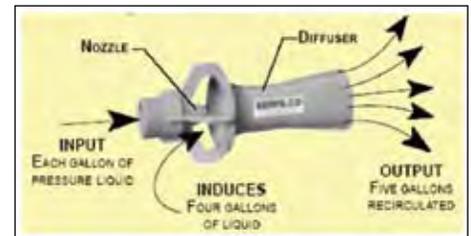
When aeration is required for the oxygen supply then the choices are somewhat limited. The compressed air economic opportunities are:

- Investigate the savings if an electric pump can replace the air driven pump. The primary limiting factors to economic use of an electric in lieu of air driven is the head pressure required (viscosity and depth) and make up of the material

- If an air operated double diaphragm pump is the proper selection, identify the lowest effective inlet pressure and add an electronic stroke optimizer. These controls can reduce the air use 40 to 50%, delivering the same throughput while incorporating automatic starts/stop if applicable
- Identify the proper pressure and flow to select the most effective compressed air supply as described earlier

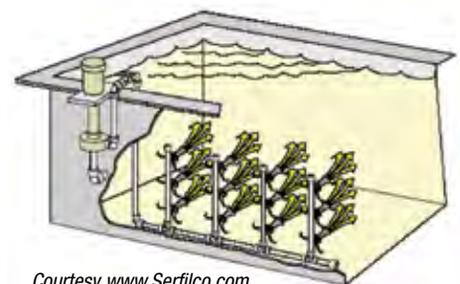
The following case studies cover some of the most prevalent opportunities.

Liquid Flow Educators



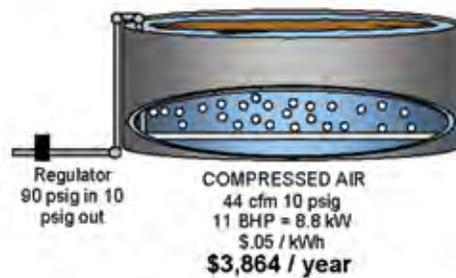
How They Work: Liquid pumped into the educator nozzles exits at high velocity, drawing an additional flow of the surrounding solution through the educator. This additional flow (induced liquid) mixes with the pumped solution and multiplies its volume five-fold. The source of the pumped liquid (input) can be a pump or filter chamber discharge.

- Eductor agitation delivers five times the pump output at each nozzle. This effectively helps deliver the required level of agitation to critical areas



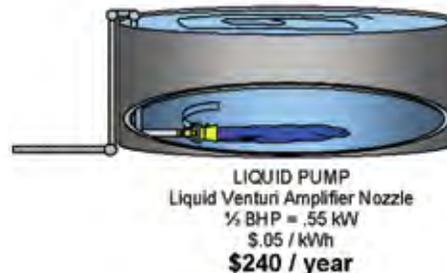
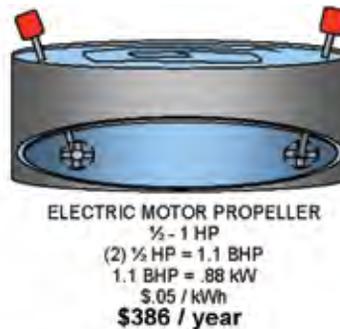
Courtesy www.Serfilco.com

- When appropriate and properly engineered and installed, this can often supply proper agitation at lower energy input



Sandpiper AODD microprocessor stroke optimizer
Courtesy of airvantagepump.com

When aeration is not needed for the oxygen content and the compressed air is used (with or a process pump) primarily for agitation, additional opportunities exist to deliver the same agitation results at a lower energy cost. Even though compressed air power is very expensive, these other actions should always be carefully evaluated on specific case by case conditions to establish an accurate operation energy cost.



Nano Super Air Nozzle for precision blowoff

The Nano Super Air Nozzle is the smallest available. EXAIR's "precision blowoff" provides optimum air entrainment for a directed high volume, high velocity airflow. The compact size permits mounting where space is limited.



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Safety Air Guns use engineered Air Nozzles to provide superior performance. Safe operation is assured along with low air consumption and noise level. Many styles and nozzles are offered. Extensions and Stay Set Hoses are available.



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Nozzle cluster, high blowing force

Many blowoff, cleaning, cooling and drying applications require high force and extensive reach. EXAIR's Super Air Nozzle Clusters deliver up to 9.8 lbs of force. Three sizes for handheld and stationary mounting are available.



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Unique flat nozzle uses patented technology

The 2" Super Air Nozzle is a highly efficient, unique flat air nozzle. Using EXAIR's patented technology, a precise amount of air is released through the thin slot, across a flat surface. The result is a wide, forceful stream of high velocity, laminar airflow. Force and flow can be easily adjusted.



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A breeze to a blast

These Safety Air Nozzles are adjustable, making them suitable for a wide variety of blowoff applications. EXAIR's design allows you to "tune in" the force and minimizing air consumption. A micrometer like dial indicates the gap setting.



www.exair.com/78/adjust.htm

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This small Super Air Nozzle costs only \$31. Installing it in place of one 1/4" copper tube can save you \$592.80 per year.

Here's how:

A 1/4" copper tube is a common homemade blowoff that consumes 33 SCFM when at a normal supply pressure of 80 PSIG. EXAIR's award winning **Model 1100 Super Air Nozzle** is 1/4 NPT and consumes only 14 SCFM at 80 PSIG.

33 SCFM (copper tube) - 14 SCFM (Super Air Nozzle) = 19 SCFM compressed air saved. For this example, the blowoff is continuous.

Most large plants know their cost per 1000 standard cubic feet of compressed air.

If you don't know your actual cost per 1000 SCF, 25¢ is a reasonable average to use.

SCFM saved x 60 minutes x cost/1000 SCF = Dollars saved per hour.

In this case, 19 SCFM x 60 minutes x .25/1000 = **28.5 cents per hour.**

28.5 cents per hour x 40 hour work week = **\$11.40 per week.**

\$11.40 per week x 52 weeks = **\$592.80 per year.**

The Super Air Nozzle pays for itself in just over two weeks.

For more information, visit www.exair.com/78/410.htm

If you would like to discuss an application, contact an Application Engineer at:



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CAC® Qualified Instructor Profile

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Mr. Van Ormer has been associated with the compressed air business for over forty years. He has been employed by several major compressor and mining equipment in major service and sales-marketing assignments. The principal focus has been compressed air equipment.

Mr. Van Ormer has visited more than 5,000 facilities and audited hundreds of compressed air systems throughout the United States and internationally. Clients include Boeing, Ford Motor, General Motors, IBM, John Deere and other Fortune 500 corporations.

In 1986, Mr. Van Ormer formed founded his independent consulting company, Air Power USA, Inc, specializing in compressed air systems. He has developed several accredited training courses for continuing education and complete curriculum for technical colleges.

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Refinery application to replace agitation air with Liquid Flow Educator

Example: The caustic production utilized two 40' tall tanks with 15' depth. Measured air flow was 240 scfm to both wastewater holding tank. The air was delivered through three 3/4" lines on three sides blowing air to keep the solids off the inside walls. There is also a 20 hp pump that continually circulates the mixture to keep the solids off the bottom and in suspension.

Total energy applied:	
240 scfm at 4 scfm input hp	60 hp
Electric motor driven pump	20 hp
Total energy	80 hp
(80 x .746 ÷ .90 @	
\$.06 kWh / 8,760 hrs yr)	66.3 kW
Estimated annual current electrical energy cost	\$34,847/yr

Project implemented: Install three educator patterns at appropriate points on the tank walls and a double set on the bottom. Total energy input 10 hp/8 kW centrifugal pump (duplex)

Total electric power operational savings (kW)	54.3 kW
Estimated annual total electric energy savings (\$.06 kWh / 8,760 hrs/yr)	\$28,540/yr
Total project cost (with installation)	\$20,000
Simple payback	8.4 months

The new educator system held the solids in suspension as required allowing appropriate storage time between cleaning and clearing.

Steel Processing Plant Filter Press Running On AODD During Complete Four Hour Cycle

The filter runs a 4-hr cycle. A 30-minute final press requires 150' of head pressure at end of each cycle. Prior to the final press, head pressure is 30 to 40 feet for 3.5 hour per cycle.

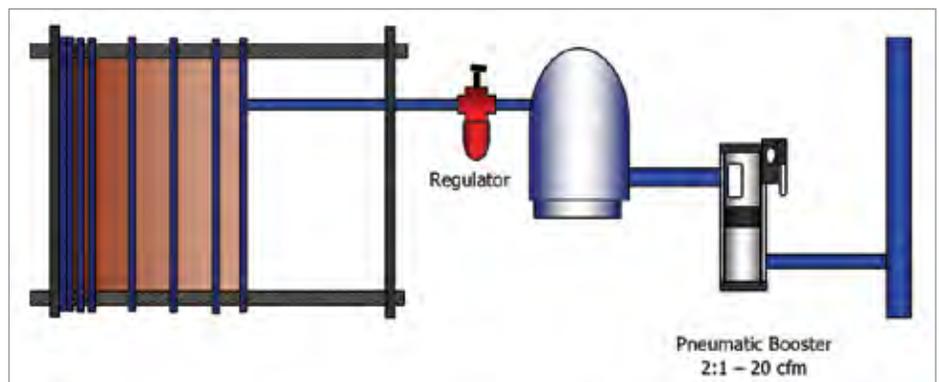
Efficiency measures such as this are taught in the Compressed Air Challenge's Fundamentals and Advanced Management seminars.

The project was to install a 2 hp electric motor driven centrifugal pump to operate the press the first 3.5 hours of the 4-hour cycle. The production processes is 24 hours a day, 7 days a week, 365 days a year with a blended power rate of \$.10 kWh.

Current air flow to 2" AODD	80 scfm
80 scfm at 90 psig at estimated input power (20 hp x .746 ÷ .90)	16.6 kW
Estimated annual electrical energy cost (16.6 kW x \$.10 kWh x 8,760)	\$14,542/yr

Modified operation

16.6 kW (x 1,095 hours (12% 8,760) x \$.10 kWh	\$1,817.70/yr
1.7 kW (2 hp motor) x 7,665 hrs/yr x \$.10 kWh	\$1,303.05/yr
Total estimated annual operating air	\$3,120.75/yr
Total savings	\$11,421.25/yr
Total project cost	\$5,000
Simple payback	5.3 months



Chlorine Plant: Two 40' Tall Wastewater Final Stage Polishing Tanks Before Release To Groundwater (Fluid Depth 30 Feet)

Current use measured 220 scfm at 90 psig compressed air regulated to 15 psig to supply agitation to maintain clarity. The air is delivered to the bottom of each tank from which it bubbles up through the water.

Current estimated electric power to produce the 220 scfm @ 4 cfm/input 55 hp
 Current estimated electric power x .746 ÷ 90 45.6 kW
 Operating cost (8,760 hrs @ \$.10 kWh) \$39,945/yr

The first alternate technology considered was utilizing the "liquid flow eductors". However,

the power to handle this tall and wide tank was 75 hp (62 kW) which was obviously not a calculated savings so the idea was abandoned. Supplying the low pressure air at 16 psig with a single-stage helical lobe blower was next explored.

A helical lobe blower using a 25 hp electric motor with 22 bhp power draw (22 x .746 ÷ 90) or 18.2 input kW will deliver 239 scfm at 15 psig. With this, the primary estimated annual energy cost is \$15,944/yr (18.2 x \$.10/kWh x 8,760 hrs) or an annual electrical energy savings of \$24,000/yr. The installed cost of the new blower package and piping was \$14,000 (up to \$28,000 depending on the package) installed. And a anticipated simple payback of 7 to 12 months.



The last case study example is in a steel mill wastewater treatment area where the limestone slurry tank is agitated with a 30 hp progressive Moyno cavity pump in a 12' tall by 8' diameter tank. The lime must be effectively kept in suspension to avoid channeling

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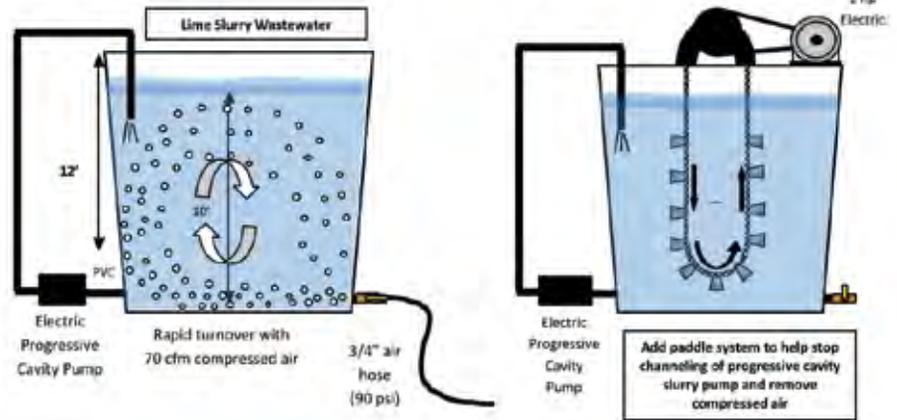
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with solids buildup around the pump entry blocking effective agitation. The solids block the recirculation volume, which accelerates the fouling factor and significantly increases the number of expensive cleanings. This can be a significant environmental and time-consuming

issue to clean out and in all probability also affecting production.

The goal was to keep the solids and in suspension until the regular scheduled maintenance time. Premature fouling was

currently avoided by adjusting fluid tank levels as required when maintenance personnel found time. This situation was not only troublesome but could lead to unplanned significant downtime with the current manpower situation.

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After the tank was cleared of solids and reset to avoid a recurrence, a 3/4" air line at 90 psig entry pressure was opened into the bottom side of the tank. The measured flow was 80 scfm, it did do the job.

Total estimated pump power
(30 hp [x .746 ÷ 90]) 24.9 kW
Total air flow 80 scfm
(80 ÷ 4 sec/input hp =
20 hp x .746 + .9) 16.6 kW
Total estimated power
utilized (8,760 operating
hours/yr @ \$.10/kWh) 41.5 kW
Total current
estimated electrical
operating energy cost \$36,354/yr

A mechanical mixing assist with paddles was added to replace the 1" air line (see drawing on previous page). This arrangement was driven by a 2 hp electric motor (2 hp x .746 ÷ .85) or 1.75 kW. This has proven to be very successful.

New configuration electrical operating energy:
30 hp progressive cavity pump 24.9 kW
Mechanical paddle pump 1.75 kW
Total electrical operating
energy power 26.65 kW
Total electrical operating
annual energy cost \$23,345/yr
Total electrical energy savings \$13,009/yr
Cost of project \$2,540
Simple payback 2.3 months

Summary

If air is needed for the wastewater treatment process and agitation alone is not enough, then there are really two choices — blower air or air compressor air. The proper choice will have a very positive impact on energy cost and, correctly applied and maintained, should enhance productivity.

The second opportunity in this case is pump selection — electric or air driven. With or without flow enhancers such as eductors, if air

operated, the use of microprocessor stroke optimized controls on AODD pumps should be considered.

If only agitation is required, it is usually to keep solids in suspension, then there are a range of options to replace or reduce compressed air usage including such mechanical devices as propellers, paddles, etc.

As you look at your wastewater system, let your imagination be your guide. As they say, "think outside the box". **BP**

For more information please contact Hank Van Ormer, Air Power USA, tel: 740-862-4112, email: hank@airpowerusainc.com, www.airpowerusainc.com

Table data and figures supplied by:
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